

## METHOD OF PRODUCING SYNTHESIS GAS

The present invention relates to a method for producing synthesis gas, comprising a reforming step in a catalytic ceramic membrane reactor (RCMC).

Synthesis gas, consisting of compounds usable in refining or petrochemicals (hydrogen, carbon monoxide) and co-produced compounds (water, carbon dioxide, methane, etc.), is generally produced by reforming hydrocarbons (natural gas, liquefied petroleum gas or LPG, naphtha, petroleum residues) or coke; this reforming is a gradual oxidation, the oxidant being water vapor, carbon dioxide, oxygen, or a mixture containing at least two of the above oxidants.

The choice of oxidant depends on the types of hydrocarbon to be reformed, on the oxidants available, and on the  $H_2/CO$  ratio required in the synthesis gas, in order, after separation and purification, to supply the needs of the local market for hydrogen, carbon monoxide or in mixture thereof (synthesis gas for the synthesis of oxo alcohols, for example).

When oxygen is used as oxidant (reforming of petroleum residues or coke, reforming of naphtha, or of lighter hydrocarbons when  $H_2$  demand is low), the oxygen must be supplied under pressure ( $10$  to  $80 \times 10^5$  Pa abs) and with high purity (over 95%), to avoid the costly removal of the inert gases (nitrogen and argon) in the synthesis gas or in the downstream processes.

In the case of reforming methods with oxygen, the cost of the oxygen accounts for a large share of the total production cost of the compounds present in the synthesis gas. The technology of catalytic ceramic membrane reactors (RCMC) allows the use of low pressure air (or of any other blend or mixture containing oxygen) as an oxygen source for hydrocarbon reforming, and eliminates the need to import (or produce) pressurized oxygen on site.

In a catalytic ceramic membrane reactor (RCMC), an oxidizing blend, also called oxidizing mixture,

containing oxygen, is supplied to one side of the ceramic membrane, and a hydrocarbon feed, essentially methane, is supplied to the other side of the membrane. The ceramic membrane used is a hybrid conductor, both  
5 ionic and electronic, and has the particular feature that when subjected to a difference in oxygen partial pressure, it allows the  $O^{2-}$  ions to pass by an ion diffusion mechanism through the oxygen vacancies in the ceramic lattice. Thus the oxygen molecules are first  
10 ionized, and the ions then diffuse through the oxygen vacancies; the oxygen ions are then deionized and the oxygen molecules react with the hydrocarbon molecules to generate synthesis gas. The presence of a catalyst, based on Ni for example, allows a very fast reforming  
15 reaction and virtually complete depletion of the oxygen, on the hydrocarbon feed side.

The diffusion of the oxygen ions through the hybrid ceramic membranes is only effective at sufficiently high temperature, typically above  $500^{\circ}\text{C}$ ,  
20 and the operating temperature must be even higher, typically above  $700^{\circ}\text{C}$ , in order to obtain a high oxygen flow; the flow of the oxygen ions through these ceramic membranes actually varies substantially with the temperature, and may have an exponential dependence on  
25 the temperature, according to the Arrhenius law.

A very large variety of hybrid conducting ceramic membranes are known today, particularly ceramics with a perovskite structure  $\text{ABO}_3$ , with dopants on the A and B sites such as  $\text{A}_x\text{A}'_{1-x}\text{B}_y\text{B}'_{1-y}\text{O}_{3-\delta}$  or  $\text{A}_x\text{A}'_x\text{A}''_{1-x-x'}\text{B}_y\text{B}'_{y'}\text{B}''_{1-y-y'}\text{O}_{3-\delta}$  (where A, A', A'' are elements of groups 1, 2, 3  
30 such as La, Sr, Ba, and B, B', B'' are transition metals such as Fe, Co, Cr, Gd, etc.).

The catalytic ceramic membrane reactor may have a planar, tubular or monolithic configuration, and is  
35 preferably of a tubular or monolithic configuration to offer sufficient mechanical strength. The hybrid conducting ceramic membranes may also be self-supporting or may bear on porous supports to obtain higher oxygen flows.

A layer of catalyst may be deposited on the oxidant side to promote higher ionization rates of the oxygen molecules.

A method for producing synthesis gas is known from  
5 US 6 077 323, using an RCMC in which the hydrocarbon  
feed is a mixture of methane-rich gaseous hydrocarbons  
to which one or more of the following constituents may  
be added: water, carbon dioxide, hydrogen, to form the  
RCMC feed gas. The gaseous hydrocarbon mixture is  
10 desulfurized but not pre-reformed before being  
introduced into the RCMC at a temperature between 510°C  
and 760°C, this temperature depending on the composition  
of the mixture. The oxidizing mixture supplied to the  
RCMC is preheated to a temperature that is not more  
15 than 111°C higher than the temperature of the feed gas  
supplied to the RCMC. The oxidizing mixture leaving  
the reactor, also called oxygen-depleted mixture or  
depleted mixture, has an RCMC outlet temperature higher  
than that of the oxidizing mixture entering the RCMC.  
20 The oxygen recovery rate in the oxidizing mixture  
supplied to the RCMC (that is, the percentage of oxygen  
consumed in the reactor) is at least 90%.

A further method for producing synthesis gas is  
known from US 6048472, comprising an RCMC, different  
25 from the previous one in that the hydrocarbon mixture  
supplied to the method is pre-reformed in an adiabatic  
reactor or in a reformer heated with the synthesis gas  
produced, or in a conventional reformer with external  
heat input in a radiant furnace, and in that the  
30 oxidizing mixture supplied to the method is air,  
possibly depleted, produced by the direct combustion of  
heating gas in a combustion chamber in which the  
pressure is preferably lower than 0.69 bar (or  $10^5$  Pa)  
gauge, or is depleted by mixing with the combustion gas  
35 with excess air from a radiant furnace.

However, the above characterizations present  
drawbacks in terms of field of application, capital  
investment, operating costs, and the cost of production  
of hydrogen and carbon monoxide, alone or in mixtures.

It is an object of the invention to propose a method and its application to remedy these drawbacks.

For this purpose, the invention relates to a method for producing synthesis gas containing hydrogen  
5 and carbon monoxide comprising the following steps:

- a step (a) of pre-reforming of a hydrocarbon mixture,

- a step (b) of reforming, in a catalytic ceramic membrane reactor (RCMC), of the pre-reformed  
10 mixture issuing from (a) by an oxidizing mixture containing oxygen to obtain raw synthesis gas containing hydrogen, carbon monoxide, carbon dioxide and water, and an oxygen-depleted mixture,

- and steps of preheating of the various fluids  
15 used,

characterized in that prior to step (b), the oxidizing mixture is heated to a temperature between 871°C and 1300°C, and preferably to a temperature of about 1000°C.

Depending on each case, the method of the  
20 invention may comprise one or a plurality of the following features, considered separately or in all technically feasible combinations:

- the hydrocarbon mixture issuing from step (a) is brought to a temperature at least 111°C lower than that  
25 of the oxidizing mixture.

Thus the preheating of the oxidizing mixture to a higher temperature serves to offset the endothermic effect of the reforming in the inlet zone of the RCMC and to maintain the membrane temperature in this zone  
30 at a level compatible with high permeability, and serves to reduce the size of the RCMC and the corresponding investment.

- the method includes a step of desulfurization of the hydrocarbon mixture prior to step (a).

- the hydrocarbon mixture is desulfurized, after  
35 the possible addition of hydrogen, at a temperature between 250°C and 450°C, and preferably at a temperature of 400°C.

- step (a) is carried out in a catalytic reactor at a temperature between 450 and 550°C, said reactor preferably being of the adiabatic type and the hydrocarbon mixture to be supplied to it is preheated  
5 to a temperature of 500°C.

Thus the method can be used to treat a mixture that may be natural gas, refinery or petrochemical waste gas, liquefied petroleum gas, naphtha, or any mixture of these various sources, containing methane  
10 and heavier hydrocarbons in any proportion.

- the depleted mixture issuing from step (b) is at a lower temperature than that of the oxidizing mixture supplied to step (b), and the temperature difference is preferably at least 75°C.

15 Thus the oxidizing mixture is a vector of heat for the benefit of the RCMC. This produces a more favorable heat balance of the RCMC, with lower total oxidation of the hydrogen and carbon, that is, lower oxygen consumption, and lower production of water and  
20 carbon dioxide. This serves to reduce the quantity of oxidizing mixture supplied to the RCMC and hence the operating cost, or to increase the oxygen content in the depleted mixture and reduce the investment. For a given feed rate, this ensures increased production of  
25 carbon monoxide and hydrogen.

- the temperature of the hydrocarbon mixture before step (b) is between 550 and 760°C, preferably 650°C.

30 - the raw synthesis gas issuing from the RCMC is at a temperature between 800°C and 1100°C, and the temperature of the depleted mixture is lower than that of said synthesis gas.

- the method uses steps of cooling, separation and/or purification, and/or of treatment of the raw  
35 synthesis gas issuing from step (b).

Thus the raw synthesis gas is cooled by any means allowing recovery of the available sensible heat, and preferably a boiler for steam production, a heat exchanger incorporating a reforming catalyst. It is

then cooled by countercurrent heat exchange with one or more fluids such as the hydrocarbon mixture, boiler water, deionized water, and possibly by heat exchange with the synthesis gas treatment modules located downstream. It is then treated to meet the specifications demanded by the market, in the modules for purification and separation of its various constituents, such as at least one decarbonation scrubber module and/or at least one module for adjustment of the  $H_2/CO$  ratio by permeation, and/or at least one module for hydrogen purification by selective adsorption.

- the oxidizing mixture supplied to step (b) is obtained by treatment of an initial oxygenated gas mixture containing 10 to 50 molar % of oxygen.

The mixture can also contain, in a non-limiting manner, water vapor, carbon dioxide and inert gases such as nitrogen and argon. The mixture may consist in particular of air, enriched air from nitrogen production units, gas from combustion carried out with a large excess of air, combustion gas supplied to (or issuing from) a gas turbine, or a mixture of these gases.

-the means employed for heat transfer during all or part of the steps of preheating of the various fluids of the method comprise at least one preheating furnace using the heat contained in the depleted mixture, and said furnace is also equipped with at least one postcombustion chamber.

The various fluids of the process means here: make-up deionized water, boiler water, the initial oxygenated mixture, the hydrocarbon mixture at the various stages of the method. The preheating steps also comprise the steps of steam generation and superheating, as well as those of the vaporization of liquid hydrocarbons. The postcombustion is advantageously supplied with heating gas and possibly with initial oxygenated gas to satisfy all the requirements of preheating, vaporization and heating of

the various fluids of the method, and in order to control its total capacity independently of the operation of the RCMC reactor.

- the oxidizing mixture is obtained by preheating  
5 the initial oxygenated gas mixture by heat exchange with the depleted mixture in a preheating furnace and/or by direct combustion of so-called primary heating gas and oxygen depletion of said initial oxygenated gas mixture in at least one combustion  
10 chamber.

The heating gas used is preferably the waste gas or gases generated by the modules for downstream treatment of raw synthesis gas which can be supplemented by modules using synthesis gas, and/or any  
15 fuel available near the unit.

- according to one particular embodiment, the initial oxygenated gas is all or part of the combustion gas available at the outlet of a gas turbine present on site, under a pressure lower than  $2 \times 10^{(6)}$  Pa  
20 (absolute), and at a temperature between 500 and 600°C.

- according to another variant of the invention, the oxidizing mixture supplied to step (b) is all or part of the combustion gas available at the outlet of the combustion chamber of a gas turbine associated with  
25 the unit, under a pressure between 20 and  $50 \times 10^5$  Pa abs and at a temperature between 1100 and 1300°C.

- advantageously, the depleted mixture issuing from step (b) is supplied to the gas turbine for the cogeneration of electrical energy.

30 - advantageously, the depleted mixture at the outlet of the gas turbine is supplied to the preheating furnace.

- advantageously, the pre-reformed hydrocarbon mixture is supplied to step (b) at a pressure differing  
35 by not more than 10% from the pressure of the oxidizing mixture supplied to said step (b).

- according to another variant of the invention, the oxidizing mixture supplied to step (b) is formed by all or part of a first combustion gas available at the

outlet of a first combustion chamber supplied with a first fraction of combustible gas and with a first oxygenated gas, for example the combustion air available at the discharge of the air compressor of an associated gas turbine.

- advantageously, the oxidizing mixture is available under a pressure between 20 and  $50 \times 10^5$  Pa abs and at a temperature between 871 and 1100°C.

- advantageously, the pre-reformed hydrocarbon mixture is supplied to step (b) at a pressure differing by not more than 10% from that of the oxidizing mixture.

- advantageously, the depleted mixture issuing from step (b) is mixed with the unused portion of the first combustion gas to feed a second combustion chamber also supplied with a second portion of combustible gas.

- advantageously, the second combustion gas issuing from the second combustion chamber is available under a pressure between 20 and  $50 \times 10^5$  Pa and at a temperature between 1100°C and 1300°C, independent of the operating temperature of the RCMC.

- the second combustion gas issuing from the second combustion chamber is preferably expanded in the gas turbine to generate electricity.

- the combustion gas issuing from the gas turbine is advantageously supplied to the preheating furnace.

- according to another variant of the invention, the initial oxygenated gas is all or part of the waste gas from a unit producing nitrogen from air, containing 25 to 40 molar % of oxygen, available under a pressure above  $1.6 \times 10^5$  Pa abs and at ambient temperature.

The invention will be better understood from a reading of the description that follows, of a method for producing a particular synthesis gas, given as a non-limiting example, with reference to Figure 1 appended hereto. Various examples of preheating modules for putting this method into practice are also presented - the preheating module being the overall



means for preheating the various fluids employed. The descriptions of these various examples are made with reference to Figures 2 to 6 appended hereto.

5 Figure 1 schematically shows the various steps of a method for the simultaneous production, from a natural gas, of highly pure hydrogen and of  $H_2/CO$  mixture which can be used for the synthesis of oxo alcohols.

10 Figure 2 shows a preheating module essentially comprising a preheating furnace and a combustion chamber suitable for putting the invention into practice.

Figure 3 shows a first variant of the preheating module incorporating an associated gas turbine.

15 Figure 4 shows a second variant integrating a gas turbine for the use of the preheating unit according to the invention.

Figure 5 shows a third variant incorporating a gas turbine for the use of the preheating unit according to  
20 the invention.

Figure 6 shows another variant of the preheating module according to the invention, using a waste gas from a nitrogen production unit present on site.

As shown in Figure 1, the hydrocarbon mixture  
25 supplied to the method consists of natural gas or GN, which, after the addition of hydrogen, is preheated to a temperature of about  $400^\circ C$  in the preheating module 1 and is desulfurized by a conventional means 2 comprising a reactor for hydrogenation of the sulfur-bearing compounds and at least one reactor for hydrogen  
30 sulfide stripping on a zinc oxide bed. After the addition of steam, the desulfurized natural gas is preheated to a temperature of about  $500^\circ C$  and is pre-reformed in an adiabatic reactor 3 containing a nickel-based catalyst. The pre-reformed mixture, a mixture of  
35 methane, hydrogen, carbon monoxide, carbon dioxide and water, is preheated to  $650^\circ C$ ; it is introduced into the reactor 4 - catalytic ceramic membrane reactor or RCMC. The preheating steps which, with the exception of the

first, are not shown in Figure 1, are carried out in the associated preheating module (a representation of this module is described below with Figure 2). Air or AP is used as initial oxygenated mixture, is compressed  
5 in a compressor 5 to a sufficient pressure to offset the pressure drops of the oxidizing mixture circuit, and is then preheated to about 1000°C before being supplied to the RCMC. This preheating is carried out in the associated preheating module shown in Figure 2.  
10 The oxidizing mixture or MO is obtained, and is then introduced into the RCMC.

In the RCMC, the oxidizing mixture MO is depleted of oxygen by giving up a part of this oxygen by permeation through the ceramic membrane. The depleted  
15 mixture MA available at the RCMC outlet is at a temperature of 925°C, and has a residual oxygen content of about 2%. The heat available in the mixture MA is then used in the preheating module.

A raw synthesis gas or GS, a product of the reforming of GN by oxygen extracted from the oxidizing mixture MO through the ceramic membrane and by the water present in the pre-reformed gas, is obtained at the outlet of the RCMC. The synthesis gas GS gives up its sensible heat in a boiler 6 generating steam in  
20 excess compared with the needs of the unit. It is then cooled in 7 by heat exchange with boiler water and deionized water, treated in a decarbonation module 8 to remove the carbon dioxide, and then sent to a drying module 9 to remove the water.

30 The gas GS is then treated in a permeation module 10 to extract a portion of the hydrogen through a polymer membrane and thereby produce a mixture with an  $H_2/CO$  ratio close to 1, an optimal ratio to supply a hydroformulation reactor and for the final production  
35 of oxo alcohols.

The hydrogen recovered in the permeate from the polymer membrane is used to regenerate the adsorbents of the drying module 9 and is compressed in a compressor 11 to supply a module 12 for selective

adsorption on adsorbents (commonly called a PSA module) which allows the production of highly pure hydrogen. The waste gas from the module 12 is used as a heating gas in the preheating module.

5       The preheating module essentially comprises a preheating furnace and a combustion chamber. It will now be described according to several variants with reference to Figures 2 to 6.

10       Figure 2 shows a preheating module in which the primary air AP used to generate the oxidizing mixture MO is compressed in an air compressor 5 to a pressure of about  $2 \cdot 10^5$  Pa abs. It is preheated to about 450°C in the preheating furnace 101 and then superheated in a combustion chamber 102 to about 1000°C by direct  
15       combustion of heating gas preferably consisting of waste fuel from the PSA module and make-up heating gas available on site, GC.

20       The oxidizing mixture MO, which leaves the combustion chamber at 1000°C, with an oxygen content of about 16 molar %, is then supplied to the RCMC 4. At the RCMC outlet, on completion of reforming, the depleted mixture MA is at a temperature of about 925°C and has a residual oxygen content of about 2 molar %; this corresponds to an oxygen extraction rate of 87.5%  
25       in the RCMC reactor. The heat available in the mixture MA, supplemented by the heat from postcombustion using a secondary make-up heating gas GC and a secondary make-up air serves to satisfy all the needs of the unit, that is in particular:

- 30       - to preheat the hydrocarbon mixture prior to its entry into the RCMC 4,  
          - to preheat the hydrocarbon mixture prior to its entry into the pre-reformer,  
          - to superheat the steam before its use inside or  
35       outside the unit,  
          - to preheat the primary air AP prior to its entry into the combustion chamber 102,  
          - to preheat the hydrocarbon mixture prior to its desulfurization,

- to preheat the boiler water.

The presence of a postcombustion chamber, of which the operation, using heating gas and secondary air, is dissociated from the RCMC, serves to satisfy all the preheating needs of the unit and to control the preheating furnace 101 independently of the RCMC.

Figure 3 shows a variant of the preheating module in which all or part of the primary air AP used to generate the oxidizing mixture MO is replaced by all or part of the effluent available at the outlet of a gas turbine 201, under a pressure lower than  $2 \times 10^5$  Pa abs and at a temperature between 450°C and 700°C, and which typically contains between 10 and 15 molar % of oxygen. The effluent from the gas turbine is then superheated in the associated combustion chamber 202 to about 1000°C by direct combustion of the heating gas preferably consisting of waste fuel from the PSA module and make-up heating gas available on site, GC.

The oxidizing mixture MO, leaving the combustion chamber 202 at 1000°C, with an oxygen content between 7 and about 12 molar %, is supplied to the RCMC 4. At the outlet of 4, on completion of reforming, the mixture MA is at a temperature of about 925°C and has a residual oxygen content of about 2 molar %; this corresponds to an oxygen extraction rate between 71% and 84% in the RCMC; the heat available in MA, supplemented by the heat from postcombustion using a secondary make-up heating gas GC and a secondary make-up air, is supplied to the preheating furnace 203 and serves to satisfy all the needs of the unit, that is in particular:

- to preheat the hydrocarbon mixture prior to its entry into the RCMC 4,
- to preheat the hydrocarbon mixture prior to its entry into the pre-reformer,

- to superheat steam before its use inside or outside the unit,
- to generate steam,
- to preheat the hydrocarbon mixture prior to its desulfurization,
- to preheat the boiler water.

The presence of a postcombustion chamber, of which the operation using heating gas and secondary air is dissociated from the RCMC, serves to satisfy all the preheating needs of the unit and to control the preheating furnace 203 independently of the RCMC.

Figure 4 shows a variant of the preheating module in which the RCMC 4 is supplied directly with all or part of the combustion gas available at the outlet of the combustion chamber 301 of a gas turbine 302, under a pressure between 10 and  $25 \times 10^5$  Pa abs., at a temperature between 871 and 1300°C, this combustion gas constituting an oxidizing mixture MO containing 10 to 15 molar % of oxygen. The RCMC 4 operates in this case under pressure. At the outlet, the depleted oxidizing mixture MA is at a pressure between 9 and  $24 \times 10^5$  Pa abs., at a temperature between 800 and 1200°C, and contains between 2 and 7 molar % of oxygen, which corresponds to an oxygen extraction rate between 30 and 87%. The depleted oxidizing mixture MA is then expanded in the gas turbine 302, coupled with the associated air compressor and with an electric power generator. The effluent available at the outlet of the turbine, under a pressure lower than  $1.2 \times 10^5$  Pa abs., is supplied to the preheating furnace 305, after the addition of a postcombustion using the waste fuel from the PSA module, a secondary make-up heating gas and a secondary make-up air. This serves to satisfy all the needs of the unit, that is in particular:

- to preheat the hydrocarbon mixture prior to its entry into the RCMC 4,
- to preheat the hydrocarbon mixture prior to its entry into the pre-reformer,

- to superheat steam before its use inside or outside the unit,
- to generate steam,
- to preheat the hydrocarbon mixture prior to its desulfurization,
- to preheat the boiler water.

The presence of a postcombustion chamber of which the operation using heating gas and secondary air is dissociated from the RCMC, serves to satisfy all the preheating needs of the unit and to control the preheating furnace independently of the RCMC.

Figure 5 shows a variant of the preheating unit in which the oxidizing mixture MO supplied to the RCMC consists of all or part of the combustion gas available at the outlet of a first combustion chamber 401 under a pressure between 10 and 25 bars abs., at a temperature between 871 and 1100°C, MO containing 10 to 15 molar % of oxygen. This first combustion chamber is supplied with a primary heating gas and with combustion air taken at the discharge of the compressor 404 coupled with a gas turbine 403. At the outlet of the RCMC, the depleted mixture MA is at a pressure between 9 and 24 bars abs., at a temperature between 800 and 1000°C and contains between 2 and 7 molar % of oxygen, which corresponds to an oxygen extraction rate between 30 and 87%. The depleted mixture MA is then superheated in a second combustion chamber 402 to a temperature close to 1200°C and expanded in the gas turbine. The effluent, available under a pressure lower than 1.2 bar abs, is supplied to the preheating furnace 405, and after addition of a postcombustion using the waste fuel from the PSA module of the unit, a secondary make-up heating gas and a secondary make-up air, serves to satisfy all the needs of the unit, that is in particular:

- to preheat the hydrocarbon mixture prior to its entry into the RCMC,

- to preheat the hydrocarbon mixture prior to its entry into the pre-reformer,

- to superheat steam before its use inside or outside the unit,

5           - to generate steam,

- to preheat the hydrocarbon mixture prior to its desulfurization,

- to preheat the boiler water.

10           The presence of a postcombustion chamber of which the operation using heating gas and secondary air is dissociated from the RCMC, serves to satisfy all the preheating needs of the unit and to control the preheating furnace independently of the RCMC.

15           Figure 6 shows a variant of the preheating unit in which the air supplied to the synthesis gas production unit is oxygen-enriched air, and is in particular the waste gas from a nitrogen production unit, containing between 25 and 40 molar % oxygen. This enriched air, or enriched primary air, is preferably made directly  
20           available at a pressure above  $1.6 \times 10^5$  Pa abs. It is preheated to about 450°C in the preheating furnace 501, is then superheated in a combustion chamber 502 to a temperature preferably of about 1000°C by direct combustion of heating gas, preferably consisting of  
25           waste fuel from the PSA module and make-up heating gas available on site and thus forms the oxidizing mixture MO.

30           The oxidizing mixture, which has an oxygen content between 20 and about 35 molar %, is then supplied to the RCMC. At the RCMC outlet, the depleted mixture is at a temperature of 915°C and has a residual oxygen content of about 2 molar %; this corresponds to an oxygen extraction rate between 90 and 95% in the RCMC reactor; the heat available in the depleted mixture,  
35           supplemented by the heat from a postcombustion chamber using a secondary make-up heating gas and a secondary make-up air, serves to satisfy all the needs of the unit, that is in particular:

- to preheat the hydrocarbon mixture prior to its entry into the RCMC,

- to preheat the hydrocarbon mixture prior to its entry into the pre-reformer,

5           - to superheat steam before its use inside or outside the unit,

- to preheat the enriched air at the outlet of the nitrogen production unit,

10           - to preheat the hydrocarbon mixture prior to its desulfurization,

- to preheat the boiler water.

The presence of a postcombustion chamber of which the operation using heating gas and secondary air is dissociated from the RCMC, serves to satisfy all the  
15   preheating needs of the unit and to control the preheating furnace independently of the RCMC.